

SIMULTANEOUS REMOVAL OF  $\text{NO}_x$  AND  $\text{SO}_x$  FROM FLUE GAS  
BY USE OF MOLTEN HYDROGENSULFATES AS REACTION MEDIA

Tsutomu SHIKADA,\* Takamasa OBA, Kaoru FUJIMOTO, and Hiro-o TOMINAGA

Department of Synthetic Chemistry, Faculty of Engineering

The University of Tokyo, Hongo, Bunkyo-ku, Tokyo 113

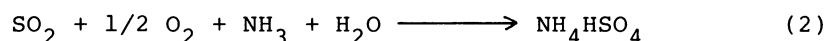
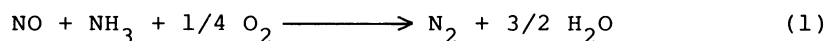
The simultaneous removal of  $\text{NO}_x$  and  $\text{SO}_x$  by reaction with ammonia from flue gas was found to be attained at temperature ranging from 150 to 200°C in molten salts of hydrogensulfates dissolving  $\text{V}_2\text{O}_5$ . The addition of transition metal sulfates such as  $\text{Ti}(\text{SO}_4)_2$ ,  $\text{Zr}(\text{SO}_4)_2$  or  $\text{CuSO}_4$  led to a marked increase in the  $\text{SO}_x$  removal.

Solid catalyzed gas phase reduction of nitrogen oxides with ammonia has been considered to be the most promising process for the removal of  $\text{NO}_x$  in flue gases emitted from stationary sources such as boiler and furnace.<sup>1-5)</sup> However, in the case of flue gases containing  $\text{SO}_2$  the latter pollutants are not removed in the method and hence another equipment is required for removing them. It is desirable as second generation for the flue gas cleaning techniques that  $\text{NO}_x$  and  $\text{SO}_x$  are simultaneously removed in the same reactor and that the reactions proceed in the temperature range from 100 to 200°C. The authors have performed the simultaneous removal of  $\text{NO}_x$  and  $\text{SO}_x$  by use of low-melting molten salts as reaction media taking into considerations the following three facts.

- 1) Supported vanadium oxide catalysts show high activities for the reduction of NO with ammonia even when they are covered with several tenth percent by weight of ammonium hydrogensulfate.<sup>6,7)</sup>
- 2) A equimolar mixture of ammonium hydrogensulfate and sodium hydrogensulfate keeps a low viscosity liquid state in the temperature range 100-200°C.
- 3) Various metal sulfates and oxides are highly soluble in the molten salt above mentioned.

It is expected in this reaction system that NO is reduced to  $\text{N}_2$ , while  $\text{SO}_2$  is fixed

as  $\text{SO}_4^{2-}$  in the reaction media, as shown in the following equations.

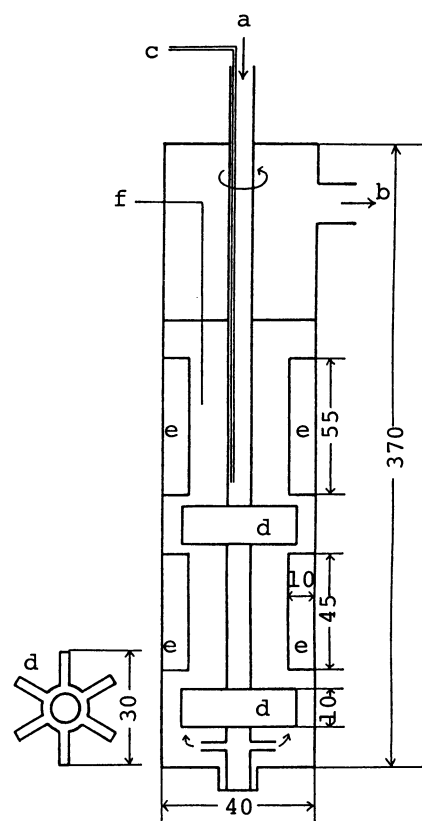


In the above equations,  $\text{O}_2$  is from excess air added to fuel for complete combustion. In the present work, it has been found that  $\text{V}_2\text{O}_5$  shows a high catalytic activity for the removal of both  $\text{NO}_x$  and  $\text{SO}_x$  and the addition of various transition metal sulfates leads to a marked increase in the removal of  $\text{SO}_x$ . The details are described here.

All chemicals used in this experiment for reaction media and catalysts were reagent grade. Catalyst consisting of  $\text{V}_2\text{O}_5\text{-NH}_4\text{Br-TiO}_2\text{-SiO}_2$  was prepared by a conventional impregnating method as described previously.<sup>8)</sup> A continuous flow type reaction apparatus was employed at atmospheric pressure. Fig. 1 shows the reactor which is an agitated bubble type one equipped with two stirrers. Reaction conditions adopted were as follows: amount of molten salt, 3.2 mol (250 ml); catalyst concentration, 5 wt%; gas flow rate, 1000 ml/min; inlet gas composition, 300 ppm of NO, 400 ppm of  $\text{SO}_2$ , 450 ppm of  $\text{NH}_3$ , 5%  $\text{O}_2$ , 10%  $\text{H}_2\text{O}$  in  $\text{N}_2$ ; stirring speed, 1200 rpm. Nitrogen monoxide and sulfur dioxide were analyzed by a chemiluminescence  $\text{NO/NO}_x$  meter and a controlled potential electrolysis  $\text{SO}_2$  meter, respectively.

The molten salt composed of 50 mol% of  $\text{NH}_4\text{HSO}_4$  and 50 mol% of  $\text{NaHSO}_4$  was employed as reaction media. The melting point of the salt was  $104^\circ\text{C}$  and the viscosity was 45 cP at  $190^\circ\text{C}$ .

In cases of reaction in a solution, the catalysis by the solvent itself or adsorption of  $\text{NO}_x$  and  $\text{SO}_x$  to the solvent is not negligible. Details of the effect of reaction media will be reported in a subsequent paper. It may be concluded that the reaction medium is virtually inactive in the removal of NO while  $\text{SO}_2$  is absorbed in the medium to some extent. Sulfur dioxide seems to be absorbed in an unstable form, probably as ammonium



a: Gas inlet, b: Gas outlet,  
c: Ammonia water, d: Stirrer,  
e: Baffle, f: Thermocouple

Fig. 1. Stirred vessel  
and impeller

sulfite in the absence of catalyst.

Table 1 shows the catalytic activities of various compounds added into the molten salt on the removal of NO and SO<sub>2</sub>. V<sub>2</sub>O<sub>5</sub>-NH<sub>4</sub>Br-TiO<sub>2</sub>-SiO<sub>2</sub> catalyst, which has been shown to be highly active at temperatures as low as 150°C for the reduction of NO with ammonia by the present authors,<sup>8)</sup> was powdered to sizes smaller than 100 mesh and dispersed in the reaction media. All other compounds which were added to the reaction media were soluble in the media. From the results shown in Table 1, V<sub>2</sub>O<sub>5</sub> showed a high activity for the removal of NO while all compounds tested, except CuSO<sub>4</sub>, showed about the same activities for removal of SO<sub>2</sub>. Sulfur dioxide is removed by reaction media alone (22.5% conversion of SO<sub>2</sub> at 160°C) and hence the effect of addition of catalyst does not seem to be so much large. However, SO<sub>2</sub> is trapped as more stable form,<sup>9)</sup> probably as ammonium hydrogensulfate in the presence of catalyst as described above. On the other hand, it is confirmed by the experiment using relatively high concentrations (2-3%) of NO, NH<sub>3</sub> and O<sub>2</sub> balanced He that NO is

Table 1 Catalytic activities of various compounds

Catalyst	Conversion (%)	
	NO	SO <sub>2</sub>
V <sub>2</sub> O <sub>5</sub> -NH <sub>4</sub> Br-TiO <sub>2</sub> -SiO <sub>2</sub>	4.7	32.5
NH <sub>4</sub> VO <sub>3</sub>	6.1	31.1
V <sub>2</sub> O <sub>5</sub>	22.4	33.0
Ti(SO <sub>4</sub> ) <sub>2</sub>	0	32.6
CuSO <sub>4</sub>	0	13.1

Medium : NH<sub>4</sub>HSO<sub>4</sub>/NaHSO<sub>4</sub> (1/1 molar ratio)

Catalyst concentration : 5 wt%

Temperature : 160°C

Table 2 Effect of sulfate additives

Additive 1. (lwt%)	Additive 2. (lwt%)	Conversion (%)	
		NO	SO <sub>2</sub>
-	-	40.0	27.8
Ti(SO <sub>4</sub> ) <sub>2</sub>	-	48.1	45.3
Zr(SO <sub>4</sub> ) <sub>2</sub>	-	45.3	52.9
CuSO <sub>4</sub>	-	40.0	59.9
Ti(SO <sub>4</sub> ) <sub>2</sub>	CuSO <sub>4</sub>	42.0	70.0
Ti(SO <sub>4</sub> ) <sub>2</sub>	Zr(SO <sub>4</sub> ) <sub>2</sub>	34.4	44.0

Medium : NH<sub>4</sub>HSO<sub>4</sub>/NaHSO<sub>4</sub> (1/1 molar ratio)

Catalyst : V<sub>2</sub>O<sub>5</sub> (5 wt%)

Temperature : 190°C

reduced by  $\text{NH}_3$  to  $\text{N}_2$  (Eq. 1).<sup>9)</sup> Thus,  $\text{V}_2\text{O}_5$  was found to be effective as the catalyst for the simultaneous removal of NO and  $\text{SO}_2$ .

The addition of various transition metal sulfates has been tried in order to increase the conversions of NO and  $\text{SO}_2$ . The experiments were carried out in the media containing 5% by weight of  $\text{V}_2\text{O}_5$  and 1% by weight of  $\text{Ti}(\text{SO}_4)_2$ ,  $\text{Zr}(\text{SO}_4)_2$  or  $\text{CuSO}_4$ . The results are given in Table 2. The addition of the sulfates promoted the removal of  $\text{SO}_2$  by about two times in  $\text{SO}_2$  conversion. The simultaneous addition of two kinds of sulfates was not so much effective. On the other hand, the addition of these sulfates was scarcely effective for the enhancement of NO removal.

In summary, the simultaneous removal of NO and  $\text{SO}_2$  was achieved at relatively high levels in the molten salts of  $\text{NH}_4\text{HSO}_4/\text{NaHSO}_4$  system containing dissolved  $\text{V}_2\text{O}_5$ . The addition of various transition metal sulfates enhanced markedly the removal of  $\text{SO}_2$ .

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